

PHYS 7810
Hydrodynamics
Spring 2024

Lecture 16

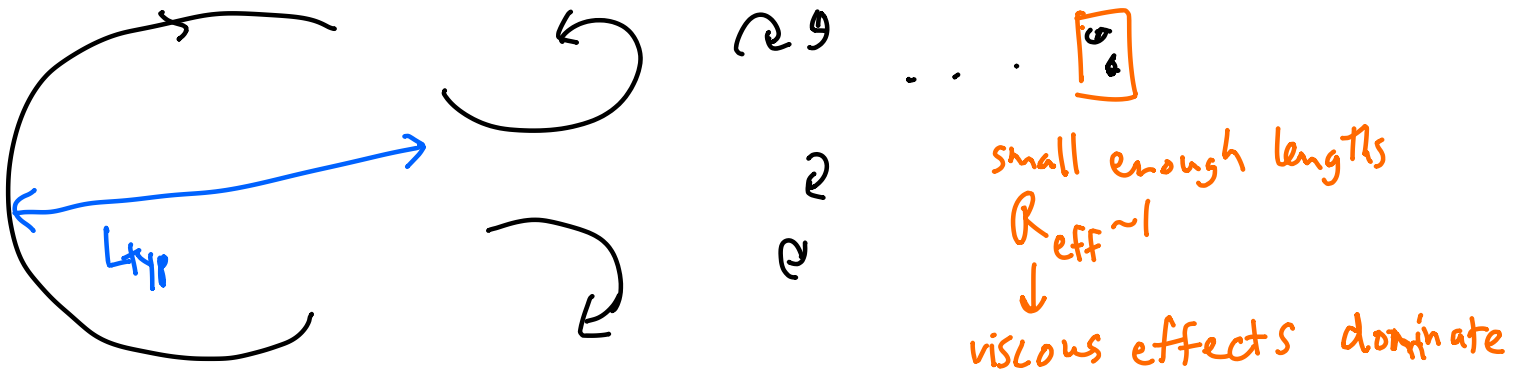
Phenomenology of turbulent flow

March 7

Recall: high Reynolds number flow $R \gg 1$:

$R = \frac{v_{typ} L_{typ}}{\nu}$, saw an instability from
Smooth/laminar flow to

turbulent flow = chaotic, multi-scale flow

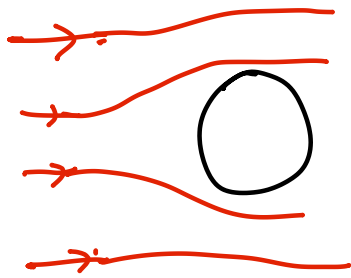


vortex/eddy splits into smaller & smaller eddies. --

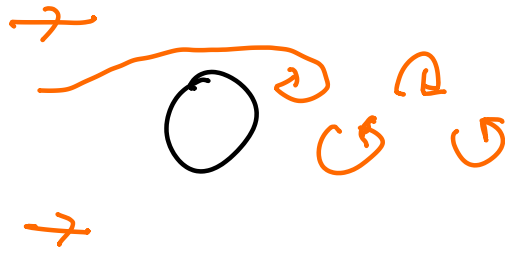
direct cascade = inject energy @ large length scales,
energy flows to small length scales.

We don't have rigorous theory for effective description
(non-chaotic) of turbulence. \Rightarrow cartoons!

Illustrative example: wake behind cylinder

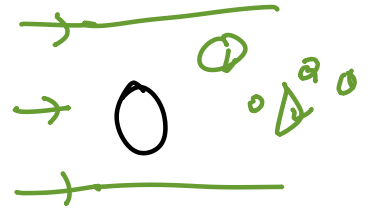


$R \sim 1$
laminar



$R \sim 100$

not turbulent,
nonlinear!



$R \sim 10^4$

turbulent.

Laminar regime: can use boundary layer theory (lec 14):

$$v_x \partial_x v_x + v_y \partial_y v_x = \nu \partial_y^2 v_x \quad [\partial_x \ll \partial_y, \delta v_x \gg \delta v_y]$$

Far from cylinder: $v_x \approx v_0 + \delta v_x$

const. far from cylinder

$$v_0 \partial_x \delta v_x + \cancel{\delta v_y \partial_y \delta v_x} = \nu \partial_y^2 \delta v_x$$

Explicit solution: $\delta v_x = \tilde{C} \frac{e^{-y^2/4(\nu x/v_0)}}{\sqrt{4\pi \frac{\nu}{v_0} x}}$

$x=0$: cylinder
 $x \gg R$: deep in wake (radius)
 approx. valid.
 integration const. TBD.

Estimate drag force/unit length:

$$F_x = \frac{d}{dt} [\text{x-momentum carried by fluid}] = \int_{-\infty}^{\infty} dy [T_{xx}(x \rightarrow -\infty) - T_{xx}(x \rightarrow +\infty)]$$

$$= \rho \int_{-\infty}^{\infty} dy [v_0^2 - (v_0 + \delta v)^2] \approx 2\rho v_0 \int_{-\infty}^{\infty} dy \delta v_x(y) = 2\rho v_0 \tilde{C}$$

Re-introduce drag coefficient (lec 14): C_D

$$C_D \sim \frac{F_x}{\frac{1}{2} \rho v_0^2 \cdot R} \quad \text{so} \quad C_D \sim \frac{\tilde{C}}{R v_0}$$

$= \text{cylinder radius}$

Usually, we expect at $R \lesssim 1$ (laminar): $C_D \sim \frac{1}{R} \times \frac{1}{\log \frac{1}{R}}$

$$F_x \sim \frac{1}{2} \rho v_0^2 R \cdot \frac{1}{R}$$

$$F_x \sim \frac{1}{2} \rho v_0 v_x \frac{1}{\log \frac{v}{v_0}}$$

Cylinder
(Stokes' Paradox)

What happens for turbulent flow?

Weak turbulence approximation:

$$v_i = \bar{v}_i(t) + \delta v_i(t, x)$$

big background
↓
small pert.
↑
statistically average over t-dep.

Expand Navier-Stokes in δv_i :

$$v_j \partial_j v_i + \frac{\partial_i p}{\rho} = \nu \partial_j \partial_j v_i$$

plug in $\bar{v} + \delta v$, avg over statistical fluctuations... (take $\overline{\delta v_i} = 0$)

$$\bar{v}_j \partial_j \bar{v}_i + \frac{\partial_i \bar{p}}{\rho} + \partial_j (\overline{\delta v_j \delta v_i}) = \nu \partial_j \partial_j \bar{v}_i$$

↳ Note incompressible $\partial_j \delta v_j = 0$.

Problem: equation for \bar{v} depends on $\overline{\delta v^2}$, \bar{v} depend on turbulent δv ...

Strategy #1: EOM for $\overline{\delta v_j \delta v_i}$?

$$\delta v_k \left[v_j \partial_j v_i + \frac{\partial_i p}{\rho} \right] = \delta v_k \nu \partial_j \partial_j v_i + (i \leftrightarrow k)$$

$$\overline{\delta v_k \delta v_j} \partial_j \bar{v}_i + \overline{\delta v_i \delta v_j} \partial_j \bar{v}_k - \bar{v}_k \partial_j \overline{\delta v_j \delta v_i} + \bar{v}_i \partial_j \overline{\delta v_j \delta v_k}$$

$$+ \overline{\delta v_k \frac{\partial_i \delta p}{\rho}} + \overline{\delta v_i \frac{\partial_k \delta p}{\rho}} + \partial_j (\overline{\delta v_j \delta v_i \delta v_k}) = \nu [\dots]$$

Solve for \bar{v} , $\overline{\delta v^2}$, $\overline{\delta v^3}$, ... until it's too annoying.

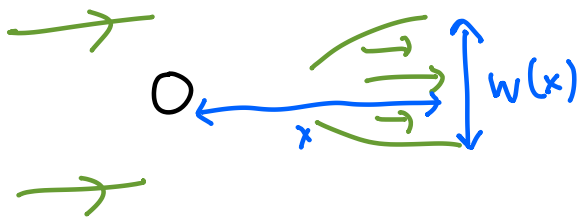
Reminiscent to kinetic theory (BBGKY) (lec 21?)

Strategy #2: Phenomenology: $\overline{\delta v_i \delta v_j} = -\nu_t (\partial_i \bar{v}_j + \partial_j \bar{v}_i)$
 ↑ "turbulent viscosity"

$$\nu_t \sim [\text{flow size}] \times [\text{velocity scale}]$$

Assume $\nu_t \gg \nu$... encoding multi-scale eddy dynamics into ν_t .

Return to wake:



$$\text{let } \delta v_x(y=0, x) = \delta v_0(x)$$

$$\text{Then } \nu_t \sim \delta v_0(x) \cdot w(x).$$

$$v_0(x) \partial_x \delta v_x = \nu_t(x) \partial_y^2 \delta v_x \longrightarrow \delta v_x \sim \tilde{C}(x) \frac{e^{-y^2/4(\nu_t x/v_0)}}{\sqrt{4\pi \nu_t x/v_0}}$$

By calculating drag force:

$$F_x = \int dy \rho [T_{xx}(x \rightarrow -\infty) - T_{xx}(x \rightarrow +\infty)] \approx \rho v_0 \tilde{C} \sim \rho v_0 \cdot \underbrace{w(x) \delta v_0(x)}_{\text{constant!} \rightarrow \nu_t}$$

Estimate by dimensional analysis: $\nu_t \sim v_0 R \cdot C_D$

Comparing width of wake in laminar vs. turbulent

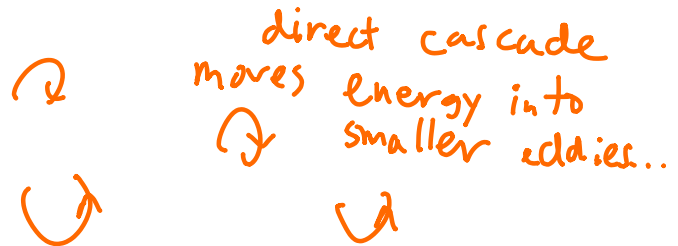
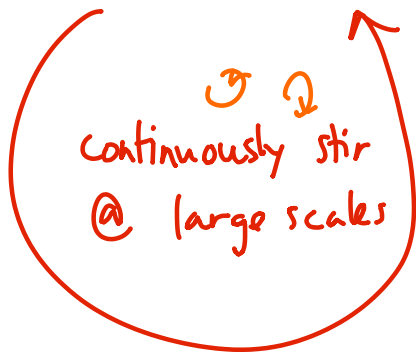
$$w \sim \sqrt{\frac{\nu x}{v_0}}$$

$$w \sim \sqrt{\frac{\nu x}{v_0}} \sim \sqrt{C_D R x} \\ \sim w_{lam} \sqrt{C_D R}$$

Since $R \gg 1$, turbulent wake much larger.

Entrainment = turbulent wake "sucks in" ambient fluid (cf HW4)

Kolmogorov (1941)'s scaling theory for isotropic, driven turbulence



Statistical steady state = injected energy @ large scales \rightarrow "flow" in k-space from small k \rightarrow large k.

$$\text{let } u(k) = \int d^3 \vec{q} \delta(|\vec{q}| - k) \frac{\rho}{2} \langle \vec{v}(-\vec{q}) \vec{v}(\vec{q}) \rangle \sim \frac{k^2}{2} \rho |\delta \vec{v}(k)|_{typ}^2$$

Dimensional analysis:

$$[u(k)] = \frac{1}{[L]^2} \cdot \frac{[M]}{[L]^3} \left[\int d^3 x e^{-i\vec{k}\cdot\vec{r}} v \right]^2 = \frac{1}{[L]^2} \frac{[M]}{[L]^3} [L]^6 \frac{[L]^2}{[T]^2} = \frac{[M][L]^3}{[T]^2}$$

fix const.

Postulate: $\frac{u(k)}{M} = \epsilon^\alpha k^\beta$

total mass \uparrow

$\hookrightarrow \epsilon = \frac{1}{M} \left(\frac{dE}{dt} \right)_{stirring}$

$\frac{\partial u(k)}{\partial t} + \frac{\partial}{\partial k} \epsilon = 0$

$$[\epsilon] = \frac{1}{[M]} \frac{[M][L]^2}{[T]^{2+1}} = \frac{[L]^2}{[T]^3}$$

Kolmogorov scaling
(\approx observed)

Combine:

$$\frac{u(k)}{M} \sim \epsilon^{2/3} k^{-5/3} \rightarrow \langle |\delta v(k)|^2 \rangle \sim \frac{u(k)}{k^2} \sim k^{-11/3}$$

Over what range of length scales do eddies exist in a turbulent flows?

Define effective Reynolds number at scale k :

$$R(k) \sim \frac{k^{-1} v_{\text{typ}}(k)}{\nu} \leftarrow \text{NOT Fourier trans}$$

By dimensional analysis, $v_{\text{typ}}(k) \sim \left(\frac{\epsilon}{k}\right)^{1/3}$.

So $R(k) \sim \frac{\epsilon^{1/3}}{\nu} k^{-4/3}$.

Turbulent flow stop at k_{max} where $R(k_{\text{max}}) \sim 1$

$$k_{\text{max}} \sim \left(\frac{\epsilon}{\nu^3}\right)^{1/4}$$

Initial flow has Reynolds $R_0 \dots$

$$\frac{R_0}{1} \sim \frac{k_{\text{min}}^{-4/3}}{k_{\text{max}}^{-4/3}} \} \rightarrow L_{\text{smallest}} \sim L_{\text{largest}} \cdot R^{-3/4}$$